



# Event-based control of input-output linearizable systems

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## 1 Introduction

The main objective of event-based control is to reduce communication between sensors, controller and actuators. A data transfer is invoked only at time instants, when an internal trigger generates an event indicating that the control error has exceeded a tolerable threshold.

A novel structure of an event-based control loop shown in Fig. 1 has been introduced in [2]. Here the dashed arrow denotes a transmission of the current plant state  $\mathbf{x}(t_k)$  from the event generator to the control input generator at the  $k$ -th event time  $t_k$ . The control input generator applies the received information to generate a control signal  $\mathbf{u}(t)$ , using a linear model of the plant. Having the same information, the event generator calculates the trajectory of the model state and compares it to the measured plant state  $\mathbf{x}(t)$ . A sufficiently large deviation between these values, caused by a disturbance  $\mathbf{d}(t)$  affecting the plant, triggers an event. Disturbance rejection is the control aim, which makes feedback of information necessary [1].

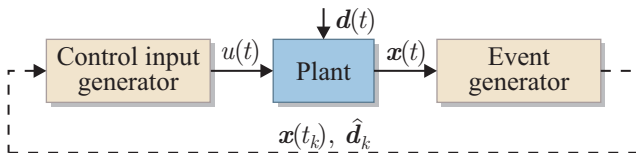


Figure 1: Event-based control loop

## 2 Project aims

The project aim is the extension of the above scheme to event-based control of nonlinear systems that are input-output linearizable. Following the idea presented in [2], the major design aim is to make the event-based control loop mimic a continuous state-feedback loop with prescribed accuracy.

The nonlinear plant that is investigated in this project is described by the affine state-space model

$$\dot{\mathbf{x}}(t) = \mathbf{f}_x(\mathbf{x}(t)) + \mathbf{g}_x(\mathbf{x}(t))\mathbf{u}(t) + \mathbf{d}_x(t) \quad (1)$$

$$\mathbf{x}(0) = \mathbf{x}_0$$

$$y(t) = h(\mathbf{x}(t)) \quad (2)$$

with single input and single output. The plant (1), (2) is assumed to be stable. With the output (2) the system is considered to have the relative degree  $r = n$ , thus,

there exists a mapping  $\phi : \mathbb{R}^n \rightarrow \mathbb{R}^n$ ,  $\mathbf{z}(t) = \phi(\mathbf{x}(t))$  that transforms the system (1), (2) into normal form

$$\begin{aligned} \dot{\mathbf{z}}(t) &= \begin{pmatrix} z_2(t) \\ \vdots \\ z_n(t) \\ b(\mathbf{z}(t)) \end{pmatrix} + \begin{pmatrix} 0 \\ \vdots \\ 0 \\ a(\mathbf{z}(t)) \end{pmatrix} \mathbf{u}(t) + \mathbf{d}(t) \\ &= \mathbf{f}(\mathbf{z}(t)) + \mathbf{g}(\mathbf{z}(t))\mathbf{u}(t) + \mathbf{d}(t) \end{aligned} \quad (3)$$

$$\mathbf{z}(0) = \mathbf{z}_0 = \phi(\mathbf{x}_0)$$

$$y(t) = z_1(t)$$

with the nonlinear functions  $b(\mathbf{z}(t))$  and  $a(\mathbf{z}(t))$  and  $\mathbf{d}(t)$  being the transformed disturbance, [4].

In a further step the project extended the results to event-based control of nonlinear systems with internal dynamics for which  $r < n$  holds, [5].

## 3 Nonlinear event-based control

A continuous state-feedback loop that serves as a *reference system* for the event-based control loop is obtained by applying to the plant (3) the state-feedback

$$\mathbf{u}(t) = \frac{1}{a(\mathbf{z}(t))} (-b(\mathbf{z}(t)) - \mathbf{k}^T \mathbf{z}(t)), \quad (4)$$

which yields the linear system

$$\begin{aligned} \dot{\mathbf{z}}(t) &= \begin{pmatrix} 0 & 1 & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & 0 & \dots & 1 \\ -k_1 & -k_2 & \dots & -k_n \end{pmatrix} \mathbf{z}(t) + \mathbf{d}(t) \\ &= \mathbf{A}\mathbf{z}(t) + \mathbf{d}(t). \end{aligned} \quad (5)$$

The static state-feedback gain  $\mathbf{k}^T$  is designed such that the continuous control loop (5) is stable and has a satisfactory disturbance rejection behavior.

The *control input generator* uses a copy of the model (5) with model state  $\mathbf{z}_s$

$$\dot{\mathbf{z}}_s(t) = \mathbf{A}\mathbf{z}_s(t) + \hat{\mathbf{d}}_k, \quad \mathbf{z}_s(t_k^+) = \mathbf{z}(t_k) \quad (6)$$

for the time interval  $t \in [t_k, t_k + 1)$ , where  $\hat{\mathbf{d}}_k$  is an estimation of the disturbance  $\mathbf{d}(t)$ , in order to generate a control input  $\mathbf{u}(t)$  according to Eqn. (4)

$$\mathbf{u}(t) = \frac{1}{a(\mathbf{z}_s(t))} (-b(\mathbf{z}_s(t)) - \mathbf{k}^T \mathbf{z}_s(t)). \quad (7)$$

The model (6) is reinitialized with the current plant state  $\mathbf{z}(t_k)$  at the time  $t_k^+$  that denotes the time instant right after the event time  $t_k$ .

The plant (3) together with the control input (7) yields the model

$$\dot{\mathbf{z}}(t) = \mathbf{A}\mathbf{z}(t) + \mathbf{e}_1\mu(\mathbf{z}(t), \mathbf{z}_s(t)) + \mathbf{d}(t), \quad \mathbf{z}(0) = \mathbf{z}_0$$

with the  $n$ -dimensional vector  $\mathbf{e}_1 = (0 \ \dots \ 0 \ 1)^T$  and the nonlinear term

$$\mu(\mathbf{z}, \mathbf{z}_s) = \left( b(\mathbf{z}) - \frac{a(\mathbf{z})}{a(\mathbf{z}_s)} b(\mathbf{z}_s) \right) + \mathbf{k}^T \left( \mathbf{z} - \frac{a(\mathbf{z})}{a(\mathbf{z}_s)} \mathbf{z}_s \right), \quad (8)$$

which is zero when the plant state  $\mathbf{z}(t)$  and the model state  $\mathbf{z}_s(t)$  coincide, but is not equal to zero if the states  $\mathbf{z}(t)$  and  $\mathbf{z}_s(t)$  diverge. The *event generator* limits the growth of the term (8) by initiating a communication to the control input generator each time when

$$|\mu(\mathbf{z}(t_{k+1}), \mathbf{z}_s(t_{k+1}))| = \bar{e} \quad (9)$$

is satisfied, with  $\bar{e} \in \mathbb{R}_+$  as the event generation threshold. At time  $t_{k+1}^+$  the model of the control input generator is reset with the state  $\mathbf{z}(t_{k+1})$  and, hence,

$$|\mu(\mathbf{z}(t_{k+1}^+), \mathbf{z}_s(t_{k+1}^+))| = 0$$

holds.

The *disturbance estimator* is implemented in the event generator and uses the model

$$\dot{\mathbf{z}}_e(t) = \mathbf{f}(\mathbf{z}(t)) + \mathbf{g}(\mathbf{z}(t))u(t), \quad \mathbf{z}_e(t_k) = \mathbf{z}(t_k)$$

to determine the estimation  $\hat{\mathbf{d}}_{k+1}$  by

$$\hat{\mathbf{d}}_{k+1} = \frac{1}{t_{k+1} - t_k} (\mathbf{z}(t_{k+1}) - \mathbf{z}_e(t_{k+1}))$$

that is used for  $t \geq t_{k+1}$ .

## 4 Analysis results

As the main analysis result, the difference between the plant state  $\mathbf{z}(t)$  of the event-based control loop and the state  $\mathbf{z}_{\text{SF}}(t)$  of the reference system

$$\dot{\mathbf{z}}_{\text{SF}}(t) = \mathbf{A}\mathbf{z}_{\text{SF}}(t) + \mathbf{d}(t), \quad \mathbf{z}_{\text{SF}}(0) = \mathbf{z}_0$$

is proved to be bounded according to

$$\|\delta(t)\| = \|\mathbf{z}(t) - \mathbf{z}_{\text{SF}}(t)\| \leq \delta_{\text{max}}$$

with

$$\delta_{\text{max}} = \bar{e} \cdot \int_0^\infty \left\| e^{\mathbf{A}\tau} \mathbf{e}_1 \right\| d\tau.$$

The second investigation concerns the communication frequency of the event-based control scheme and uses the value  $\zeta$  as the minimal deviation between the plant state  $\mathbf{z}$  and the model state  $\mathbf{z}_s$  for which the condition (9) is satisfied:

$$\zeta := \min_{\mathbf{z}, \mathbf{z}_s} \|\mathbf{z} - \mathbf{z}_s\|, \quad \text{s. t. } |\mu(\mathbf{z}, \mathbf{z}_s)| = \bar{e}.$$

For a bounded disturbance

$$\|\mathbf{d}_\Delta(t)\| = \left\| \mathbf{d}(t) - \hat{\mathbf{d}}_k \right\| \leq d_{\Delta \text{max}}$$

the event-based control loop is shown to have a minimal inter-event time  $T_{\text{min}}$  that is bounded from below by

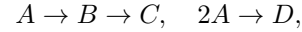
$$T_{\text{min}} \geq \bar{T}$$

with  $\bar{T}$  satisfying

$$\int_0^{\bar{T}} \left\| e^{\mathbf{A}\tau} \right\| d\tau = \frac{\zeta}{\bar{e} + d_{\Delta \text{max}}}.$$

## 5 Experimental example

The event-based control approach shall be applied to control a chemical reaction in a continuous stirred tank reactor (Fig. 2). The tank is fed by a reactant  $A$  with temperature  $\vartheta_{\text{in}}$  and concentration  $c_{\text{in}}$ . The temperature  $\vartheta_c$  of the cooling jacket is affected by the cooling power  $\dot{Q}$ . The liquid in the tank is supposed to be at a constant level. The reactions inside the liquid are described by the ‘‘van de Vusse’’ reaction scheme



comprising the reaction of educt  $A$  to the desired product  $B$  and the parallel reactions to the byproducts  $C$  and  $D$ .

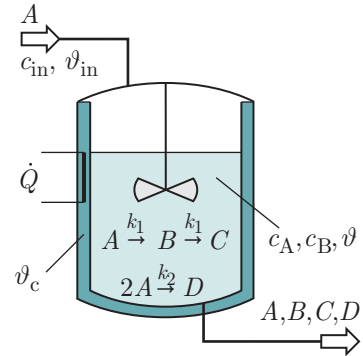


Figure 2: Scheme of the continuous stirred tank reactor

The control aim is to keep the concentrations  $c_A$  and  $c_B$  of the reactant  $A$  and the product  $B$  constant. A disturbance of the process is realized by a variation of the cooling power  $\dot{Q}$  that has an impact on the chemical reaction via the temperature  $\vartheta$ .

## References

- [1] J. Lunze. *Regelungstechnik 1*, Springer, Berlin 2008
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- [5] C. Stöcker and J. Lunze. Event-based control of nonlinear systems: An input-output linearization approach. submitted to *CDC/ECC 2011*.